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CANTEL HARDONEMENTS IN THE CONTERBION OF CHEMICAL MOLETING	0.00	CONTRACTOR AND

(54) Title: IMPROVEMENTS IN THE CONVERSION OF CHEMICAL MOIETIES

(57) Abstract

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Approximation of the property

A process for the conversion of a chemical moiety, which may be gascous, liquid or a solid in fluidised form, in which the chemical moiety is reacted with a plasma or with a reagent generated by the interaction of plasma with another component, which may be a solid.



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iety, which may be gaseous, liquid or a solid in fluidised form, in which the igent generated by the interaction of plasma with another component, which

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This invention relates to improvements in or relating to processes for converting fluidised chemical moieties.

Where this activation energy is high, the reaction is to be carried out at lower pressures, e.g. atmospheric pressure or sub-atmospheric The reactions We have now found a new method of supplying the energy therefor, require less energy and are safer. The ability to carry out the reactions at lower temperatures and pressures also means that cheaper materials and simpler methods of construction can be used in the construction of In general, reactions need energy to initiate the reaction. commonly carried out at high temperature and/or pressure. and/or lower temperatures. which enables reactions the reaction vessels. pressure

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Alternatively improved results may be obtained at the higher temperature and/or pressure.

is in a fluid phase and said moiety is reacted with a In accordance with the present invention, there is provided an improvement in processes for the conversion of a chemical molety characterised in that the chemical molety plasma or with a reagent generated by the interaction of the plasma with another component. The process may involve the use of a catalyst.

herein, relates to the conversion of a material to a desired product and not merely to surface modification. It is also to be understood that the invention relates to is not derived from the same molecule, and thus does not It is to be understood that the term conversion, as used conversion of one chemical by treatment with a plasma which relate, for example, to plasma polymerisation.

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is to improvements in or relating to ing fluidised chemical moleties.

n energy is high, the reaction is at high temperature and/or pressure.

new method of supplying the energy fons to be carried out at lower spheric pressure or sub-atmospheric wer temperatures. The ability actions at lower temperatures and that cheaper materials and simpler on can be used in the construction of

d results may be obtained at the i/or pressure.

present invention, there is provided rocesses for the conversion of a sterised in that the chemical moiety and said moiety is reacted with a ent generated by the interaction of r component. The process may involve

d that the term conversion, as used the conversion of a material to a t merely to surface modification. It tood that the invention relates to ical by treatment with a plasma which he same molecule, and thus does not o plasma polymerisation.

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The molety may be an element or a compound and may be gaseous or liquid or it may be a solid which is in fluidised form. Where the chemical molety is a liquid, e.g. through which the plasma is bubbled, it may be provided as such or as an aerosol, in which case the carrier gas may be or comprises the gas that is excited to plasma.

In the embodiment where the molety is reacted with a reagent generated by the action of the plasma on another component, the plasma may be directed, for example, onto the surface of a solid to produce reactive species which react with the molety. The solid may be a catalyst, for example. Alternatively, the reactive species may be generated from the action of the plasma on a liquid.

Plasma is normally generated from a gas; however, a liquid may also be used. For example, water may be excited to form plasmas of hydrogen and oxygen.

Any suitable means may be employed for generating the plasma. For example, it may be generated by DC glow discharge, AC electric field, plasma torch and heat, all of which may be pulsed. The heat may be generated by laser.

Alternating currents for generating the AC plasmas are preferably those having a frequency of 1-10¹⁴Hz, more preferably 10³-10⁹Hz. It will be understood, however, that in some countries the frequencies that may be used are limited, e.g. because of the risk of interference with radio transmissions. For example, in Great Britain, a frequency of 13.56MHz is set aside by the Government for such experiments and will not therefore interfere with radio transmissions. Other frequencies can be used, provided that the Government is advised of the intention to use these frequencies.

the plasma is bubbled, it may be as an aerosol, in which case the in element or a compound and may be or it may be a solid which is in comprises the gas that is excited to re the chemical moiety is a liquid,

here the moiety is reacted with a a may be directed, for example, onto id to produce reactive species which γ . The solid may be a catalyst, for vely, the reactive species may be the action of the plasma on another tion of the plasma on a liquid. merated from a gas; however, a liquid for example, water may be excited to gen and oxygen. may be employed for generating the e, it may be generated by DC glow c field, plasma torch and heat, all of The heat may be generated by laser.

It will be understood, however, that ne frequencies that may be used are For example, in Great Britain, a ; is set aside by the Government for for generating the AC plasmas are ving a frequency of $1-10^{12} \mathrm{Hz}$, more e of the risk of interference with will not therefore interfere with

ernment is advised of the intention to Other frequencies can be used,

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such frequencies may give rise to alternating or periodic discharges are advantageous when the power input has to be Frequencies of less than 1 Hz may also be used. However, minimised or to provide additional control of the reaction. discharge rather than a continuous plasma.

are suitable. However, the pressure used is dependent on the power loadings. Therefore, if a sufficiently high atmospheric pressure. Pressures of from 100 to 10-3 torr power loading is available, it is possible to excite gas to plasma that is generated by alternating current at radionormally generated from gases at plasma at a pressure above 100 Torr, if desired. frequency is

plasma or plasma torch are often generated at a variety of However, plasmas generated by other means such pressures ranging from sub- to super- atmospheric.

result in power loss and a reduction in the efficiency of Where the reaction vessel is large, as in an industrial scale reaction, it is preferable to generate the plasma at likelihood of the plasma varying in intensity across so as to reduce antinodes of plasma intensity may be created which If higher frequencies are used, nodes lower frequencies such as 40kHz the process. vessel.

A mixture of more than one plasma may be employed and where more than one gas or liquid is excited to plasma, this may be effected before or after mixing,

reactions, it is particularly useful for converting toxic jases, such as are present in internal combustion engine While the process of the invention may be applied to toxic waste products. Either or both of the toxic gas and to nonexhaust gases and gaseous industrial emissions, conversions generally, and more particularly

than 1 Hz may also be used. However, give rise to alternating or periodic rathan a continuous plasma. Such ageous when the power input has to be ie additional control of the reaction.

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r, the pressure used is dependent on
Therefore, if a sufficiently high
lable, it is possible to excite gas to
above 100 Torr, if desired.

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erated by other means such as arc h are often generated at a variety of m sub- to super- atmospheric. preferable to generate the plasma at ich as 40kHz so as to reduce the isma varying in intensity across the frequencies are used, nodes and intensity may be created which may and a reduction in the efficiency of

one plasma may be employed and where liquid is excited to plasma, this may after mixing.

f the invention may be applied to y, and more particularly gaseous icularly useful for converting toxic resent in internal combustion engine seous industrial emissions, to non-Either or both of the toxic gas and

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the gas employed to convert it to a non-toxic product may be converted to plasma.

Internal combustion engine exhaust gases and other exhausts from hydrocarbon burning consist mainly of CO, NOx and gaseous hydrocarbons. The NOx can be detoxified by reaction with CO or unburned hydrocarbons to give N, and CO₂. Excess carbon monoxide and unburned hydrocarbon fuel are normally oxidised to CO₂ and water.

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Examples of the detoxification of industrial gaseous emissions include the denaturing of NOx to water and nitrogen gas using hydrogen plasma, the dehalogenation of organic molecules using hydrogen plasma and the removal of odour from industrial emissions such as the emissions from fat rendering, glue and size manufacturing, tanning, fish meal processing, polyvinyl chloride and polyurethane manufacturing and cutting, food manufacturing, coffee roasting, manure processing and meat processing industries. Some of these detoxification reactions may require the presence of a catalyst.

Exhaust gases and gaseous industrial emissions commonly include fine particulate matter dispersed in the gas. The process of the present invention may be used to convert the particular moleties to more acceptable gaseous products, to soluble products which can then be removed from the gas e.g. by washing, or to liquids which can be separated from the gas. For example, carbonaceous material such as soot can be treated with an oxygen plasma to form carbon dioxide.

Some reactions have such a high energy of activation that they have to be carried out at very high temperature and/or be initiated by free radicals even in the presence of a catalyst. We have now found that if such reactions are carried out in the presence of plasma in accordance with

convert it to a non-toxic product may

angine exhaust gases and other exhausts rning consist mainly of CO, NOx and The NOx can be detoxified by unburned hydrocarbons to give N, and nonoxide and unburned hydrocarbon fuel 1 to CO, and water. stoxification of industrial gaseous ydrogen plasma, the dehalogenation of ing hydrogen plasma and the removal of l emissions such as the emissions from and size manufacturing, tanning, fish olyvinyl chloride and polyurethane utting, food manufacturing, coffee dification reactions may require the he denaturing of NOx to water and essing and meat processing industries.

ch can then be removed from the gas t invention may be used to convert the o more acceptable gaseous products, to o liquids which can be separated from a, carbonaceous material such as soot an oxygen plasma to form carbon aseous industrial emissions commonly ate matter dispersed in the gas.

radicals even in the presence of a now found that if such reactions are such a high energy of activation that resence of plasma in accordance with ed out at very high temperature and/or

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Alternatively, the results achieved using such high litro compounds, nitriles, oximes, carboxylic aromatic this invention, the need for high temperature or free temperature and/or free radical initiators may be improved. Reactions which may be carried out in this manner include, out are not limited to, hydrogenations such as of olefins, acetylenes, aldehydes, ketones, acíds, anhydrídes, esters, reductive alkylation, reductive amination, dehalogenation, disproportionation migration, decomposition, carbonylation, decarbonylation, selective oxidation, acetoxylation and gas purification. compounds, anilines, phenols and derivatives hydrogenolysis, isomerization, тау initiators

Whilst the present invention has particular advantages when used with reactions which have previously required high cemperature and/or free radical initiation, it may also be used for reactions which do not have such a high activation

co-pending application, entitled "Improvements in Processes involving Catalyst", filed on the same day as the present the surface of the catalyst with a gas in the form of a Many reactions are promoted by catalysts that become application, such catalyst may be regenerated by contacting plasma. Processes may therefore be envisaged in which both the reactant mixture for a catalysed gaseous reaction and As described in our the catalyst regeneration employ plasma. deactivated with the passage of time.

the regeneration of the catalyst in a second, subsequent period. Two reactors may be employed in parallel, in one which the regeneration is taking place. When the catalyst of which the reaction is taking place and in the other of In the second reactor has been regenerated, the operations catalysed reaction may take place in one time period and In accordance with one aspect of such processes,

ntion has particular advantages when hich have previously required high radical initiation, it may also be h do not have such a high activation

romoted by catalysts that become ssage of time. As described in our entitled "Improvements in Processes lled on the same day as the present yst may be regenerated by contacting alyst with a gas in the form of a therefore be envisaged in which both or a catalysed gaseous reaction and on employ plasma.

take place in one time period and e catalyst in a second, subsequent say be employed in parallel, in one is taking place and in the other of is taking place. When the catalyst as been regenerated, the operations

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in the two reactors may be reversed so that the reaction is effected over regenerated catalyst in the second reactor while the catalyst of the first reactor is regenerated. Of course, more than two reactors may be used with appropriate switching arrangements.

In some cases, the gas or gases required to regenerate the catalyst may already be included in, or readily generated from, the gaseous mixture which is to be treated in the presence of the catalyst. In such cases, a self-contained procedure can be envisaged where in one step the gaseous component, or at least one of the gaseous components, employed in the regeneration of the catalyst and in another step the same mixture is treated to convert to plasma at least one of the other gases of the mixture, being a gas involved in the reaction which is promoted by the catalyst. The first step may also involve a reaction to generate a required gas, e.g. the gas which is to be converted to plasma, where it is not already present as such in the reaction mixture.

An example of such a case is the detoxification of exhaust gas emissions from motor vehicles. For example, the catalyst employed in the catalytic converters fitted to motor vehicles for the detoxification of the exhaust gases tend to be deactivated with time due to poisoning by lead and/or phosphorus which are employed in additives for motor fuels.

Lead can be removed from the surface of the catalyst by the action of chlorine plasma which converts it to a soluble salt and phosphorus can be removed by the action of hydrogen plasma; the reactions proceeding according to the following equations:

C1, -----> 2C1 (chlorine plasma)

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lay be reversed so that the reaction is the first reactor is regenerated. Of reactors may be used with appropriate rated catalyst in the second reactor Ęs.

isaged where in one step the gaseous the gaseous er gases of the mixture, being a gas lso involve a reaction to generate a the gas which is to be converted to not already present as such in the is or gases required to regenerate the be included in, or readily generated xture which is to be treated in the lyst. In such cases, a self-contained eration of the catalyst and in another e is treated to convert to plasma at ion which is promoted by the catalyst. ast one of the gaseous components, to plasma convert t t

ne detoxification of the exhaust gases ad with time due to poisoning by lead case is the detoxification of exhaust For example, the the catalytic converters fitted to ch are employed in additives for motor motor vehicles.

rom the surface of the catalyst by the lasma which converts it to a soluble can be removed by the action of reactions proceeding according to the

---> 2C1 (chlorine plasma)

H2 ----- 2H (hydrogen plasma) PbC12 + 2C1 ------ PbC14 Pb + 2Cl ----- PbCl, P + 3H ----- PH₃ Thus, where halogenated compounds, for example CC1, and H2 are present in the exhaust gases or can be generated from appreciated that the regeneration of the catalyst may be achieved using the exhaust gas itself by treating it to convert one or both of the chlorine and hydrogen components in these gases, it will or gases present thereof to plasma. a gas

therefore be designed wherein the catalyst is regenerated on board the vehicle, using the vehicle engine's exhaust Catalytic converter systems for motor vehicles emissions. Where the plasma or plasmas employed for the catalyst regeneration do not interfere with the reaction which is being promoted by the catalyst, it may even be possible to effect the catalysed reaction and the regeneration of the catalyst simultaneously.

important industrial process is in the Haber process for the catalytically promoted synthesis of ammonia from nitrogen and hydrogen. The catalyst is usually trivalent iron. Known methods require that the reaction is carried out at high temperatures and pressures such as 670K and 150 Where the reaction is carried out according to the present invention, lower temperatures and pressures can An example of an application of the present invention to an be used thus reducing the risk of explosion, the energy required to carry out the synthesis and its cost. to 350 atm.

In practice, a stoichiometric mixture of nitrogen and hydrogen is excited to plasma by any means in the presence

.----- PbC1,

-----> PbCl₂

--> 2H (hydrogen plasma)

-----> PH₃

ust gases or can be generated from nt in these gases, it will be generation of the catalyst may be nust gas itself by treating it to compounds, for example CC1, and H2 he chlorine and hydrogen components

sing the vehicle engine's exhaust ystems for motor vehicles can herein the catalyst is regenerated

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lasmas employed for the catalyst erfere with the reaction which is talyst, it may even be possible to action and the regeneration of the

oted synthesis of ammonia from The catalyst is usually trivalent quire that the reaction is carried and pressures such as 670K and 150 action is carried out according to ocess is in the Haber process for ower temperatures and pressures can tion of the present invention to an he risk of explosion, the energy e synthesis and its cost.

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ometric mixture of nitrogen and lasma by any means in the presence

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admixture of hydrogen and nitrogen is excited prior to being passed over the catalyst. In this case, the catalyst will be located in a separate zone to that in which the into contact with the catalyst at the desired temperature gases are excited to plasma. The plasma is then brought and pressure. If desired, one only of the hydrogen and of the catalyst to produce the ammonia. Alternatively, the nitrogen is converted to plasma.

unsaturated organic compound in an inert solvent such as invention where the moiety to be converted is a liquid. A plasma of oxygen is bubbled through a solution of the methanol, glacial acetic acid, ethyl acetate, hexane or chloroform at a temperature which is preferably in the region of -20°C but which may be at or above ambient the cleavage of a carbon-carbon double bond by oxidation compounds is an example of an application of the present temperature. The ozone is produced in the oxygen plasma. with ozone followed by hydrolysis to yield

poisoned with sulphur and phosphorus. The mixture is exposed to a plasma of an inert gas to decompose the aluminium hydride to aluminium and hydrogen species. These species then react with the sulphur and phosphorus poisons The plasma may convert the chemical moiety to a reactive substance which then takes part in a further reaction. For example, aluminium hydride may be mixed with a catalyst to form a mixture of products, namely aluminium sulphide, aluminium phosphide, hydrogen sulphide and phosphine.

Alternatively, the catalyst may be mixed with zinc oxide and exposed to a hydrogen plasma. Both reactive poisons, such as mercaptan and thiol compounds, and unreactive poisons, such as aromatic sulphur compounds can be removed :rom the catalyst surface by this means.

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An example of the chemical moiety being converted to

rbon-carbon double bond by oxidation olety to be converted is a liquid. A compound in an inert solvent such as by hydrolysis to yield carbonyl ple of an application of the present bubbled through a solution of the etic acid, ethyl acetate, hexane or erature which is preferably in the which may be at or above ambient ne is produced in the oxygen plasma. ot the chemical moiety to a reactive dride may be mixed with a catalyst r and phosphorus. The mixture is takes part in a further reaction. For of an inert gas to decompose the luminium and hydrogen species. These th the sulphur and phosphorus poisons products, namely aluminium sulphide, ydrogen sulphide and phosphine. talyst may be mixed with zinc oxide nd thiol compounds, and unreactive atic sulphur compounds can be removed ogen plasma. Both reactive poisons, face by this means. emical molety being converted to a

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reactive substance where the moiety is a liquid is where a catalyst poisoned with hydrocarbons and lead is suspended the oxygen and chlorine species formed will respectively oxidise the hydrocarbons and convert the lead to a washable mixture is exposed to plasma of oxygen and/or inert gas, in or is in contact with dichlorine heptoxide. lead salt.

ere the molety is a liquid is where a h hydrocarbons and lead is suspended with dichlorine heptoxide. When the

ine species formed will respectively uns and convert the lead to a washable

) plasma of oxygen and/or inert gas,

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1. A process for the conversion of a chemical moiety characterised in that the chemical moiety is in a fluid phase and said moiety is reacted with a plasma or with a reagent generated by the interaction of plasma with another component.

- A process according to Claim 1, wherein the moiety is in liquid form and the liquid is in the form of an aerosol.
- A process according to Claim 1, wherein the chemical moiety is a fluidised finely divided solid.
- 4. A process according to Claim 5, wherein the moiety is in gaseous form and is also provided in the form of plasma.
- 5. A process according to any one of Claims 1 to 4, wherein the plasma is generated by an AC electric field, by DC glow discharge, by a laser or by plasma torch.
- 6. A process according to Claim 5, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from $10^3 \rm Hz$ to $10^9 \rm Hz$.
- 7. A process according to Claim 5, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from $10^9 \rm Hz$ to $10^{13} \rm Hz$.
- A process according to any one of Claims 1 to 7, wherein said another component is a solid.
- 9. A process according to Claims 8, wherein said another component is a catalyst.
- 10. A process as claimed in any one of Claims 1 to 9 comprising the detoxification of a gaseous industrial

the conversion of a chemical moiety it the chemical moiety is in a fluid y is reacted with a plasma or with a the interaction of plasma with another

_ Demonstration and T

ing to Claim 1, wherein the molety is a liquid is in the form of an aerosol.

ing to Claim 1, wherein the chemical ifinely divided solid.

ing to Claim 5, wherein the moiety is a also provided in the form of plasma.

ding to any one of Claims 1 to 4, generated by an AC electric field, by a a laser or by plasma torch.

ing to Claim 5, wherein the plasma is ; electric field and wherein the .s supplied at from $10^3 \rm Hz$ to $10^9 \rm Hz$.

ing to Claim 5, wherein the plasma is selectric field and wherein the s supplied at from $10^9 \rm Hz$ to $10^{12} \rm Hz$.

ding to any one of Claims 1 to 7, component is a solid.

ing to Claims 8, wherein said another st.

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laimed in any one of Claims 1 to 9 xification of a gaseous industrial

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emission or internal combustion engine exhaust.

- 11. A process according to any one of Claims 1 to 9, wherein the reaction is carried out in the presence of a catalyst.
- 12. A process according to Claim II, wherein the catalyst is located in a zone remote from that in which the plasma is generated.
- 13. A process according to any one of Claims 1 to 12, wherein the reaction of the chemical moiety with the plasma generates a reactive species which takes part in a second reaction.
- 14. A process according to any one of Claims 1 to 13, wherein the conversion is carried out as a continuous, semi-continuous or batch process.

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- 11 -

oustion engine exhaust.

ig to any one of Claims 1 to 9, carried out in the presence of a to Claim 11, wherein the catalyst ote from that in which the plasma

to any one of Claims 1 to 12, he chemical moiety with the plasma ses which takes part in a second

to any one of Claims 1 to 13, is carried out as a continuous, process.

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AMENDED CLAIMS [received by the International Bureau on 24 January 1994 (24.01.94); original claims 1-14 amended; new claims 15-25 added (3 pages)]

- 1. A process for the conversion of a chemical moiety characterised in that the chemical moiety is in a fluid phase and said moiety is reacted with a plasma, or with a reagent generated by the interaction of plasma with another component, said conversion being effected in the presence of a catalyst, said catalyst being regenerated by in situ treatment with plasma.
- 2. A process according to Claim 1, wherein the conversion of the chemical moiety and the catalyst regeneration are carried out simultaneously.
- A process according to Claim 1 or 2, wherein the moiety is in liquid form and the liquid is in the form of an aerosol.
- 4. A process according to Claim 1 or 2, wherein the chemical moiety is a fluidised finely divided solid.
- 5. A process according to Claim 1 or 2, wherein the moiety is in gaseous form and is also provided in the form of plasma.
- 6. A process according to any one of Claims 1 to 5, wherein the plasma is generated by an AC electric field, by DC glow discharge, by a laser or by plasma torch.
- 7. A process according to Claim 6, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from 10³Hz to 10³Hz.
- 8. A process according to Claim 6, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from 10°Hz to 1012Hz.

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 A process according to any one of Claims 1 to 8, wherein said another component is a solid.

AMENDED CLAIMS ional Bureau on 24 January 1994 (24.01.94); ended; new claims 15-25 added (3 pages)]

ion of a chemical moiety characterised in that the ase and said moiety is reacted with a plasma, or with teraction of plasma with another component, said presence of a catalyst, said catalyst being regenerated

m 1, wherein the conversion of the chemical moiety : carried out simultaneously.

laim 1 or 2, wherein the moiety is in liquid form and erosol. n 1 or 2, wherein the chemical moiety is a fluidised

n 1 or 2, wherein the moiety is in gascous form and olasma. ne of Claims 1 to 5, wherein the plasma is generated glow discharge, by a laser or by plasma torch.

6, wherein the plasma is generated by an AC electric ; current is supplied at from 103Hz to 109Hz. 6, wherein the plasma is generated by an AC electric current is supplied at from 109Hz to 1012Hz.

ne of Claims 1 to 8, wherein said another component

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10. A process according to Claim 9, wherein said another component is the catalyst.

11. A process as claimed in any one of Claims 1 to 10 comprising the detoxification of a gaseous industrial emission or internal combustion engine exhaust.

12. A process according to any one of Claims 1 to 11, wherein the catalyst is located in a zone remote from that in which the plasma is generated. A process according to any one of Claims 1 to 12, wherein the reaction of the chemical moiety with the plasma generates a reactive species which takes part in a second reaction 13

A process according to any one of Claims 1 to 13, wherein the conversion is carried out as a continuous, semi-continuous or batch process. 14

phase and is reacted with a plasma, or with a reagent generated by the interaction of A process for the detoxification of gaseous industrial emissions or internal combustion engine exhaust characterised in that the emission or exhaust is in a fluid plasma with another component, in the presence of a metallic catalyst. 15.

16. A process according to Claim 15, wherein the emission or exhaust is in liquid form and the liquid is in the form of an aerosol.

17. A process according to Claim 15, wherein the emission or exhaust is a fluidised finely divided solid. 18. A process according to Claim 15, wherein the emission or exhaust is in gaseous form and is also provided in the form of plasma.

13 1. E), wherein said another component is the catalyst.

e of Claims 1 to 10 comprising the detoxification internal combustion engine exhaust.

of Claims 1 to 11, wherein the catalyst is located 1 the plasma is generated.

me of Claims 1 to 12, wherein the reaction of the enerates a reactive species which takes part in a

one of Claims 1 to 13, wherein the conversion is ontinuous or batch process.

tion of gaseous industrial emissions or internal rised in that the emission or exhaust is in a fluid or with a reagent generated by the interaction of the presence of a metallic catalyst.

- 1 15, wherein the emission or exhaust is in liquid f an aerosol.
- 5, wherein the emission or exhaust is a fluidised
- $\boldsymbol{5},$ wherein the emission or exhaust is in gaseous \boldsymbol{m} of plasma.

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19. A process according to any one of Claims 15 to 19, wherein the plasma is generated by an AC electric field, by DC glow discharge, by a laser or by plasma torch.

- 20. A process according to Claim 19, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from 10³Hz to 10⁹Hz.
- 21. A process according to Claim 19, wherein the plasma is generated by an AC electric field and wherein the alternating current is supplied at from 10⁹Hz to 10¹²Hz.
- 22. A process according to any one of Claims 15 to 21, wherein said another component is a solid.
- 23. A process according to Claim 22, wherein said another component is the catalyst.
- 24. A process according to any one of Claims 15 to 23, wherein the reaction of the emission or exhaust with the plasma generates a reactive species which takes part in a second reaction.
- 25. A process according to any one of Claims 15 to 24, wherein the conversion is carried out as a continuous, semi-continuous or batch process.

any one of Claims 15 to 19, wherein the plasma is field, by DC glow discharge, by a laser or by plasma Claim 19, wherein the plasma is generated by an AC alternating current is supplied at from 103Hz to 103Hz.

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Claim 19, wherein the plasma is generated by an AC alternating current is supplied at from 109Hz to 1012Hz.

any one of Claims 15 to 21, wherein said another

laim 22, wherein said another component is the catalyst.

plasma generates a reactive species which takes part in any one of Claims 15 to 23, wherein the reaction of the

o any one of Claims 15 to 24, wherein the conversion is semi-continuous or batch process.

INTERNATIONAL SEARCH REPORT

PCT/GB 93/01641

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